REMARKS

With the entering of this amendment, claims 1-16 will be pending claims 1-10 are withdrawn from consideration by the examiner as being directed to a non-elected invention and claim 11 has been amended.

The examiner is requested to enter this amendment since it is directed to eliminating the rejections under 35 USC 112 and distinguishing over the art by clarifying the claim language. The amendments do not introduce any new issues and thus do not require a further search or consideration of new issues by the examiner.

Claim 11 has been amended to clearly indicate that there is a gaseous reactant and a liquid reactant and a solid which is a catalyst and that a reaction occurs by reacting the gaseous reactant and liquid phase reactant together in a gas phase and liquid phase. While their may be more than one gaseous reactant and liquid reactant, there are at least one of each which produce a reaction. It is believed that these amendments negate all the specific objections raised by the examiner in the 35 USC 112, second paragraph rejections of claims 11-16.

Claims 11, 12, 15 and 16 stand rejected as anticipated by WO 98/16463 (equivalent to U.S. 6,375,920.)

This rejection is not applicable to these amended claims for the reasons recited in the previous amendment dated August 21, 2003.

The claims clearly indicate that the process involves a gaseous reactant and a liquid reactant which produces a reaction. The reference process which is directed to two gaseous reactants, accordingly, does not anticipate these claims.

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Additionally, the amended claims also distinguish from WO 98/16463 by indicating that the process is operated under "isothermal conditions".

The rejection of claims 13 and 14 as being obvious over WO 98/16463 is not applicable for the reasons recited in the amendment dated August 21, 2003.

In view of the above amendments and comments the case is now clearly in condition for allowance.

Favorable action by the examiner is solicited.

Should a fee be required, kindly charge Deposit Account No. 11-0345.

Respectfully submitted,

KEIL & WEINKAUF

Edward J. Smith Reg. No. 24,074

1350 Connecticut Ave., N.W. Washington, D.C. 20036

(202)659-0100

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COPY OF CURRENT CLAIMS

- (withdrawn) Apparatus for carrying out reactions involving a gaseous phase, a and a solid phase being a catalyst, which comprises the steps of, comprising
- a dispersing element (6) for dispersing a gas phase in a liquid phase to generate a reaction fluid,
- at least one reactor (1) which possesses an inlet (31, 41), an outlet (43) and a reactor space bounded by heat-removing walls which are spaced apart substantially uniformly along the main flow axis of the reaction fluid, and which is fitted with catalyst-coated metal fabric (20, 32), and
- a feed line (7) which routes the reaction fluid from the dispersing element (6) to the reactor inlet (31,41) and is sufficiently short that the degree of dispersion of the reaction fluid does not substantially change in the course of the passage through the feed line.
- 2. (withdrawn) Apparatus as claimed in claim 1, wherein the metal fabric (20, 32) is knitted metal fabric.
- (withdrawn) Apparatus as claimed in claim 1, wherein the metal fabric (20, 32) is knitted metal fabric.
- (withdrawn) Apparatus as claimed in claim 1, where the dispersing element (6) is a liquid jet gas compressor.
- 5. (withdrawn) Apparatus as claimed in claim 1, wherein the reactor (1) is constructed as a heat exchanger.
- 6. (withdrawn) Apparatus as claimed in claim 5, wherein the reactor (1) is

EVERTZ et al., Ser. No. 10,070,805 constructed as a plate type heat exchanger.

- 7. (withdrawn) Apparatus as claimed in claim 5, wherein the reactor (1) is constructed as a spiral type heat exchanger.
- 8. (withdrawn) Apparatus as claimed in claim 5, wherein the walls in the reactor are spaced from 1 to 3 mm apart.
- 9. (withdrawn) Apparatus as claimed in claim 5, wherein the walls in the reactor are spaced from 2 to 20 mm apart.
- (withdrawn) Apparatus as claimed in claim 5, wherein the walls in the reactor are spaced from 4 to 10 mm apart.
- 11. (currently amended) A process for carrying out <u>a reaction under isothermal</u>

 <u>conditions</u> reactions involving a <u>gas gaseous</u> phase, <u>containing</u> a <u>liquid phase</u>

 and a solid phase, where at least one <u>gaseous</u> reactant, is <u>gaseous</u> and one

 reactant <u>a</u> liquid <u>phase containing</u> at least one liquid reactant and <u>a</u> the solid

 phase <u>being</u> is a catalyst, which comprises the steps of
 - generating a reaction fluid by dispersing the gas phase containing the at

 least one gaseous reactant in the liquid phase, containing the at least one

 liquid reactant and producing a reaction thereby, passing the generated

 reaction fluid through a reactor whose reactor space is equipped with

 woven or knitted metal fabrics coated with catalyst,
 - transferring the heat of reaction through the reactor to a <u>cooling</u> fluid medium on the reaction wall surface facing away from the reactor space, and

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- separating the reaction fluid into gas phase and liquid phase.
- 12. (original) A process as claimed in claim 11, operated with separate partial recycling of gas phase and/or liquid phase.
- 13. (original) A process as claimed in claim 11, wherein the superficial liquid velocity in the reactor is from 100 to 66 m³/m²-h).
- 14. (original) A process as claimed in claim 11, wherein the superficial gas velocity is from 0.5 to 15 cm/s.
- 15. (original) A process as claimed in claim 11, wherein the reaction fluid in the reactor is under a pressure of from 0.1 to 200 bar.
- 16. (original) A process as claimed in claim 11, wherein the reaction fluid in the reactor has a temperature of from 25 to 250°C.